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(54) Title: A PROCESS FOR THE PREPARATION OF TABLETS FROM PHARMACEUTICALLY ACTIVE SUBSTANCES HAVING UNFAVOURABLE TABLETTING PROPERTIES WITH A GRANULATING LIQUID COMPRISING MICROCRYSTALLINE CELLULOSE

(57) Abstract: The invention refers to a process for the preparation of tablets that can be well compressed and have good mechanical strength from pharmaceutically active ingredient(s) having unfavourable tabletting properties. In the process of the invention a granulating liquid is used which is a suspension of 5-30 % of microcrystalline cellulose - 90% of which have a particle size that is lower than 50 Sg(m)m, and the amount of the microcrystalline cellulose refers to the final tablet mass in water and/or ethanol and/or isopropanol, and said suspension may contain also a part of the ingredients of the granules in dissolved form.

A PROCESS FOR THE PREPARATION OF TABLETS FROM PHARMACEUTICALLY ACTIVE SUBSTANCES HAVING UNFAVOURABLE TABLETTING PROPERTIES WITH A GRANULATING LIQUID COMPRISING MICROCRYSTALLINE CELLULOSE

Field of the invention

The invention refers to a process for the preparation of tablets that can be well compressed and have good mechanical strength from pharmaceutically active ingredient(s) having unfavourable tabletting properties by admixing the pharmaceutically active ingredient(s) to conventional carriers used in tabletting, preferably binding agent(s) and/or filling agent(s) and/or disintegrating agent(s) and/or surfactant(s), granulating the mixture in the presence of a granulating liquid by a kneading or a fluidization spraying process, and tabletting the granules obtained using further carriers conventionally employed in tabletting, preferably lubricant(s) and/or disintegrating agent(s) and/or glident(s).

Background of the invention

In the therapeutical use of pharmaceutical active ingredients, the most generally employed closage form is the tablet (and coated tablet). The pharmaceutical firms manufacture a nearly inappreciable amount of tablet all over the world, taking into consideration that the tabletting capacity of a modern tabletting machine is about 500 000 pieces in every hour. In the same

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time, these tabletting machines of high performance need granules that can be tabletted without any problem since a huge damage may arise due to a short-fall of production when a machine stops or owing to the formation of an anormous amount of rejects when tablets of unsatisfactory quality are manufactured. Therefore, prior to tabletting, the active ingredients have to be transformed to granules that are suitable for tabletting. In general, such granules consist of particles having a size of 0.1-1.0 mm, and are prepared during different so-called preparatory procedures. A detailed description of these procedures can be found in the corresponding textbooks [such as Rácz, I. and Selmeczi, B.: Gyógyszertechnológia (Pharmaceutical Technology), Vol. 1-3, Medicina, Budapest, 1994].

Principally, three kinds of preparatory process are employed:

- technology in which powders are mixed,
- dry granulation technology,
- wet granulation technology.

In case of the technology in which powders are mixed, the active ingredient is homogenized with carriers that can be easily tabletted. This technology is also called direct tabletting. The drawback of this process is that it can be employed only in a small part of the active ingredients that can be compressed also without carriers or are used in a low dose.

In case of the dry granulation technology, the active ingredient

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is homogenized with carriers that can be easily tabletted, the mixture obtained is compressed (formed to briquettes or pretabletted), the compressed material is ground, passed through a sieve, admixed to further carriers and tabletted. Again, this technology is employed only in a small part of the active ingredients - usually the ones that are sensitive to drying - since the tabletting properties of the active ingredients cannot be suitably improved by this method.

In case of the wet granulation technology, the active ingredient or, if desired, the mixture of the active ingredient and carriers used in tabletting is wetted with the so-called granulating agent. In this way, the surface of the solid particles will be covered by a film that forms from the materials dissolved in the granulating agent, and this film will be dried to the surface in the drying step that follows wetting. Thus, in the latter technology, the surface properties of the particles consisting of the active ingredient and the other solid carriers added to the active ingredient before granulation can be significantly - and, from the point of view of tabletting, favourably - changed. Recently, in the majority of cases, the wet granulation technology is employed as the preparatory process for tabletting.

In the wet granulation process, from the active ingredient(s) or, if desired, from a mixture of the active ingredient(s) and carriers which have a starting particle size of mainly lower than 0.1 mm, granules are prepared the 70 % by mass of which have a particle size of 0.1-1.0 mm. Although the wet granulation

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technology can be carried out in various equipments, recently, the vortex flow or fluidization spraying granulation technology is exclusively used.

The vortex flow granulation equipments contain a mixer element driven by two separate motors. The main mixer puts the material to be granulated in vortex motion, hence the name of the equipment, and kneads, aggregates the solid powders with the granulating liquid added into the equipment. The so-called cutting head that rotates at high speed grinds the aggregates formed during kneading. The resulting wet granules can be dried in a separate drier or in the granulation equipment itself.

In case of the fluidization spraying granulation technology, the particles to be granulated are in fluid state in the fluidization column owing to an air stream, and the granulating liquid is sprayed onto the particles. The wetted particles aggregate, and the granules can be dried in the apparatus when further granulating solution is not sprayed anymore.

Prior to granulation, various carriers are added to the active ingredient to obtain suitable tablet properties. Based on the role that influence the tablet properties, the carriers can be classified as follows:

- filling or diluting agents,
- binding agents,

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- disintegrating agents that facilitate the dissolution of the active ingredient.

The filling or diluting agents are used, in case of the preparation of low dose tablets each containing lower than 100 mg of active ingredient, to increase the tablet mass, while in other cases to improve the tabletting properties of the active ingredient. Most often the following filling or diluting agents are employed: lactose monohydrate, mannitol, cellulose, microcrystalline cellulose, calcium hydrogen phosphate (anhydrous or dihydrate).

The binding agents are used to form a bond among the small particles of the active ingredients and carriers when preparing the granules on the one part, and to improve the mechanical strength of the final tablets on the other. The binding agents used in the wet granulation should dissolve in the granulating liquid. In general, the binding agents are high molecular natural or artificial materials, for example gelatin, maltodextrin, arabic gum, poly(vinyl pyrrolidone), cellulose ethers and esters (methyl cellulose, ethyl cellulose, hydroxypropyl methyl cellulose), acrylate copolymers, poly(vinyl acetate), poly(vinyl butyrate) etc. However, the bond between the particles can be also formed with the solutions of low molecular agents (such as lactose, mannitol, sucrose, glucose) or even with the active ingredients dissolved in the granulating liquid. In this case, the bond among the primary particles of the granules is provided by the active ingredient or carrier crystallizing among the particles.

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The disintegrating agents and auxiliary agents that facilitate the dissolution of the active ingredient, respectively, are hydrophilic agents that swell in aqueous medium, thus, provide for the disintegration of the tablets to granules, and the disinregration of the granules to primary particles in aqueous medium. On the other hand, this class of carriers includes surfactants that facilitate wetting of the tablets and granules, and increase the solubility of the active ingredient. The most important disintegrating agents are the following: various starches (maize, potato, wheat), sodium or calcium salt of carboxymethyl starch, sodium or calcium salt of carboxymethyl cellulose, hydroxypropyl cellulose, poly(vinyl pyrrolidone) etc. It is to be noted that the starch and cellulose ethers used as disintegrating agent contain a lower amount of functional groups in comparison with the ones used as binding agent, thus, the starch and cellulose ethers suitable as disintegrating agent only swell in water, while the ones useful as binding agent form a colloidal solution in water.

In practice, the solution of the binding agent(s), low molecular carrier(s) or active ingredient(s) is used as the granulating liquid, however, also a solvent or solvent mixture can be used which dissolves a part or all of the components in the powder mixture to be granulated.

In addition to the carriers mentioned above, usually using a technology in which powders are mixed, also glidents and

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lubricants (anti-friction and anti-adhesion agents) are admixed to the granules prepared as described above to facilitate tabletting. The glidents promote the granules to fill the matrix slit of the tabletting machine more evenly, thus, reducing the mass deviation of the tablets. The anti-friction agents reduce the friction between the material to be tabletted or the final tablet and the matrix wall, while the anti-adhesion agents eliminate the adherence between the tabletting dies and the surface of the tablets and provide the bright surface of the tablets.

Most frequently, colloidal silica and talc are used as glident, magnesium stearate, stearic acid and hydrogenized vegetable oils are employed as anti-friction agent, and magnesium stearate and talc are used as anti-adhesion agent. In the development of the tabletting technology of a pharmaceutically active agent, the grade and amount of the above carriers as well as the granulation technology should be selected to obtain tablets that satisfy the quality requirements.

The quality of tablets are regulated essentially by the pharmacopeial prescriptions. Although these prescriptions are not entirely unified yet, however, primarily those of the European (Ph. Eur) and US (USP) Pharmacopeias are considered as a standard for the international pharmaceutical industry.

At present, the most severe prescriptions referring to tablet parameters that are critical from the point of view of tabletting

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are as follows:

Tablet parameter	Prescription of	Prescription of
	Ph.Eur.	USP
Deviation of tablet	under 80 mg: ± 10	
mass	%	none
·	80-250 mg: ± 7.5	
	%	
	above 250 mg: ± 5	
	%	
Active ingredient	nominal value $\pm5\%$	nominal value ± 10
content of the tablet		%
Deviation of active	average value ± 15	nominal value ± 15
ingredient content	%	%
		relative deviation:
		not more than 1 %
Disintegration time	not more than 15	it depends on the
	min.	specific preparation
Dissolution of the	there is no general	75-85 % in 30-60
active ingredient	requirement	min.
		depending on the
		specific preparation
Friction loss	not more than 1 %	not more than 1 %
Tablet strength ^x	there is no	there is no
	requirement	requirement

^x As to tablet strength, a value of 1 Mpa is advised for the

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tensile strength in the literature. (Tensile strength is the ratio of the collapsing force and the surface area that ruptures.)

However, in case of several active ingredients, it is extremely difficult to attain the values prescribed for the critical tablet parameters because of the unfavourable tabletting properties of the active ingredients.

The following properties of the active ingredients influence the tablet manufacture unfavourably:

- strong adhesion,
- weak cohesion,
- bad solubility in water.

In case of strongly adhesive materials, partly high friction forces appear during compression which may cause the damage of the tablet when it is pressed out from the die, partly the tablets adhere to the surface of the die, thus, uneven tablet surface is obtained. In principle, the latter problem could be eliminated by the addition of a large amount of anti-friction agent, however, large amounts of anti-friction agents would reduce the tablet strength, prolong the disintegration of the tablets in aqueous medium (owing to the hydrophobic character of the anti-friction agents) and slow down the dissolution of the active ingredient, thus, the tablets obtained would not correspond to the quality prescriptions.

In case of materials having weak cohesion, the required tablet strength cannot be achieved by the compression. In principle, this problem could be eliminated by the addition of a large amount of binding agent, however, large amounts of binding agents would unacceptably prolong the disintegration of the tablets in aqueous medium and slow down the dissolution of the active ingredient, thus, again, the tablets obtained would not correspond to the quality prescriptions.

If the active ingredient has a bad solubility in water, the strong adhesion or weak cohesion thereof creates problem in an increased degree since the use of large amounts of both antifriction agents and binding agents makes impossible to achieve the fast dissolution of the active ingredient.

Because of the above difficulties, several patented processes have been developed for the preparation of the tablets of certain active ingredients having unfavourable tabletting properties.

In UK-P No. 1 445 983 the preparation of allopurinol tablets is described. To reduce the sizes of tablets containing 55-79 % by mass of active ingredient, 15-35 % by mass of indifferent filling agent (such as mannitol, dicalcium phosphate, microcrystalline cellulose or, preferably, lactose), 5-15 % by mass of disintegrating agent (such as alginic acid, sodium starch glycolate, guar gum, calcium carboxymethyl cellulose or, preferably, starch) and 1-10 % by mass of granulating agent (such as starch paste, gelatin, methyl cellulose or, preferably, poly(vinyl pyrrolidone) are employed.

In DE-P No. 342 774, the preparation of tablets containing 80-90 % by mass of allopurinol is described. The tablets comprise, in addition to the active ingredient, 5-8 % by mass of microcrystalline cellulose, 3.5-7 % by mass of a disintegration agent based on starch, furthermore binding agent (such as poly(vinyl pyrrolidone) and glident (such as colloidal silica).

According to both documents mentioned above, the active ingredient is granulated as follows: the active ingredient, filling agent and disintegrating agent are mixed in powdered form, the mixture obtained is granulated using the aqueous solution of the binding agent [poly(vinyl pyrrolidone)], and, after drying and sieving, glidents are added followed by tabletting.

HU-P No. 191 384 describes the preparation of fast dissolution tablets containing at least 80 % by mass of alpha-methyldopa. 5-15 % by mass of microcrystalline cellulose as the filling agent, 1-3 % by mass of sodium carboxymethyl cellulose as the disintegrating agent, furthermore a mixture of 0.5-5 % by mass of polyvinyl butyral and 0.5-5 % by mass of acrylate copolymer as binding agent are used in the process.

According to US-P No. 5,281,421, for the preparation of fast dissolution tablets containing gemfibrozil, 1-4 % by mass of a surface active agent having a HLB (hydrophilic lipophilic balance) value of 10-50 are used.

For the preparation of fast dissolution tablets containing

gemfibrozil, HU-P 212 428 describes the use of 0.05-0.5 % by mass of diotilane [bis(2-ethyl-hexyl)-sodium-sulfosuccinate] as the surface active agent.

According to HU-P No. 196 710, ciprofloxacin tablets or capsules of fast dissolution can be prepared by using a dry binding agent based on microcrystalline cellulose, a disintegrating agent based on starch, a glident, a further disintegrating agent based on a cellulose derivative and/or poly(vinyl pyrrolidone) and a lubricant. In the examples used for comparison in the description, the fast dissolution of ciprofloxacin is provided by the presence of disintegrating agents, maize starch and poly(vinyl pyrrolidone).

In case of the last four documents, the granulation technology is performed by granulating the powder mixture of the active ingredient, binding agent(s) and optionally the disintegrating agent(s) with a solution of the binding agent (HU-P No. 191 384, US-P No. 5,281,421, HU-P No. 196 710) or only with the granulating solvent (HU-P No. 196 710).

Thus, up to now, the processes for improving the tabletting of pharmaceutically active ingredients have advised the use of more and more efficient binding agents, and increasing the amount of the binding agents and the anti-friction agents, respectively. In the same time, these steps have an unfavourable influence on the disintegration of the tablets and the dissolution rate of the active ingredient, respectively. To

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counteract this influence, the use of surface active agents is proposed. However, these may be also harmful since they can facilitate the absorption of toxic agents that are eventually present in the gastrointestinal system. Therefore, from the point of view of manufacturing pharmaceutical tablets, a process would be highly advantageous which would allow to use as low amount of binding agents (indispensable for the mechanical strength of the tablets) and anti-friction agents (essential for the compression) as possible and simultaneously improve the disintegration time of the tablets and the dissolution rate of the active ingredient.

When studying the tabletting technology of various pharmaceutically active ingredients, it has been found that even from active ingredients having unfavourable tabletting properties it is possible to produce tablets having good mechanical strength and to use only a low amount of high molecular binding agents and hydrophobic anti-friction agents, thus, obtaining fast disintegrating tablets from which the active ingredient dissolves readily, when the granulation is carried out with a granulating liquid which is a suspension of 5-30 % of microcrystalline cellulose, 90 % of which have a particle size that is lower than 50 μ m (the amount of the microcrystalline cellulose refers to the final tablet mass).

Several sorts of microcrystalline cellulose have been used in the tablet manufacture since about 1970 mainly as filling agent. At first, they have been employed primarily in case of direct

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compression technologies, however, at present, they are widely used also in wet granulation processes. For different purposes different grades of microcrystalline cellulose are commercially available which differ from each other in particle size, density and wet content [Wade, A. and Weller, P.J.: Handbook of Pharmaceutical Excipients, The Pharmaceutical Press, London, 1994].

The various grades of microcrystalline cellulose are distinguished by code numbers. Based on the code numbers, the characteristic physical parameters of each grade and the field of use advised by the manufacturers are given in the following table.

Grade	Mean size in mm	Wet conten t in %	Densit y in g/cm ³	Field of use
101	50	max. 5	about 0,30	This type is used most frequently for wet granulation and direct tabletting or spheronization.
102	100	max. 5	about 0,33	Better gliding properties than grade 101, mainly for direct compression.
103	50	max. 3	about 0,30	Similar to grade 101, recommended for materials of lower wet content which are sensitive to wetness.
105	25	max. 5	about 0,23	Inert carrier for materials that do not crystallize. Sedimentation agent in dispersion and preparation of suppositories.
112	100	max. 3	about 0,33	Similar to grade 102, recommended for materials of lower wet content which are sensitive to wetness.
200	180	max. 5	about 0,38	This grade has the best gliding properties, it is recommended for direct tabletting.
301	. 50	max. 5	about 040	This grade is similar to grade 101 but has higher density and better gliding properties, it is recommended for direct tabletting.
302	100	max. 5	about 40	This grade is similar to grade 102 but has higher density and better gliding properties, it is recommended for direct tabletting.
12	160	max. 5	about 0,39	Good gliding properties, recommended for direct tabletting.
20	30	max. 5	about 0,21	Similar quality and use than those of grade 105.

According to the state of art, the different grades of microcrystalline cellulose described above are used by admixing the microcrystalline cellulose to the active ingredient and, if desired, other carriers in powdered form, and, in case of direct tabletting, the powder mixture is tabletted. If the gliding

and/or compressing properties of the powder mixture is not sufficient, wet granulation is carried out. In the latter procedure, the powder mixture is granulated with the solution of a binding agent and/or with a suitable solvent, the granules obtained are dried, sieved, mixed with a glident and tabletted.

Thus, the possible use of microcrystalline cellulose in aqueous or aqueous alcoholic suspensions for improving the tabletting technologies of active ingredients having unfavourable tabletting properties has not been known in the prior art.

Summary of the invention

Thus, according to the invention, tablets that can be well compressed and have good mechanical strength are prepared from pharmaceutically active ingredient(s) having unfavourable tabletting properties by admixing the pharmaceutically active ingredient(s) to conventional carriers used in tabletting, preferably binding agent(s) and/or filling agent(s) and/or disintegrating agent(s) and/or surfactant(s), granulating the mixture in the presence of a granulating liquid by a kneading or a fluidization spraying process, and tabletting the granules obtained using further carriers conventionally employed in tabletting, preferably lubricant(s) and/or disintegrating agent(s) and/or glident(s), in which process the granulating liquid is a suspension of 5-30 % of microcrystalline cellulose - 90 % of which have a particle size that is lower than 50 μ m, and the amount of the microcrystalline cellulose refers to the final tablet

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mass - in water and/or ethanol and/or isopropanol, and said suspension may contain also a part of the ingredients of the granules in dissolved form.

Description of the preferred embodiments

In the preparation of the granules, conventional carriers that are used in tabletting are employed. Preferably, such carriers include one or more binding agent(s) (the total amount thereof is 1-10 % of the final tablet mass, in general), optionally one or more filling agent(s) (if used, in general, the total amount thereof is not higher than 50 % of the final tablet mass, however, depending on the active ingredient content, the total amount thereof can be also 99 %), one or more disintegrating agent(s) (the total amount thereof is 1-40 % of the final tablet mass, in general) and optionally one or more surfactant(s) (if used, the total amount thereof is not higher than 5 % of the final tablet mass, in general).

For tabletting the final granules, in general, further carriers conventionally used in tabletting are employed. Such carriers include, preferably, one or more lubricant(s) (the total amount thereof is 0.1-5 % of the final tablet mass, in general), optionally one or more disintegrating agent (if used, the total amount thereof is not higher than 20 % of the final tablet mass, in general), and optionally one or more glident(s) (if used, the total amount thereof is not higher than 3 % of the final tablet mass, in general).

In the process of the invention, the microcrystalline cellulose content of the final tablet is wholly or partially suspended in the granulating liquid and this suspension is used for the granulation. The granulation liquid can be water, ethanol, isopropanol or any mixtures thereof or a solution of the binding agents or any other material(s) that are present in the final tablet in water, ethanol, isopropanol or any mixtures thereof. For the preparation of the suspension, only microcrystalline celluloses having low particle size that is 90 % of cellulose particles are smaller than 50 μ m (such as grades 20, 105, 101, 103), preferably 90 % of the cellulose particles are smaller than 25 μ m (such as grades 20, 105) are employed since microcrystalline celluloses of higher particle size or higher density cannot be suspended suitably.

In the preparation of the suspension of the microcrystalline cellulose, the binding agents to be dissolved in the solvent or solvent mixture include binding agents generally used in tablet preparation or filling agents. For example, hydrophilic polymers such as poly(vinyl pyrrolidone) or vinylpyrrolidone/vinylacetate copolymer, poly(vinyl alcohol), poly(ethylene glycol), cellulose ethers such as ethyl cellulose, hydroxyethyl cellulose, hydroxypropyl methyl cellulose, sodium carboxymethyl cellulose, starch hydrolysates such as maltodextrin, protein hydrolysates such as gelatin etc. can be dissolved. Of the filling agents, sugar and sugar alcohols such as lactose, glucose, sucrose, mannitol, sorbitol etc. can be dissolved, primarily.

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Thus, according to the process of the invention, the microcrystalline cellulose content of the tablet to be prepared is wholly or partially suspended in water and/or ethanol and/or isopropanol. In the thus-obtained granulating liquid, a part of the components of the granules, generally 30 % by mass thereof at the most, can be also dissolved. These components are dissolved either one by one, in any order of sequence or simultaneously. It is also possible to dissolve the active ingredient or a part thereof in the granulating liquid.

The composition of the granulating suspension is suitably adjusted to obtain a liquid that can be still poured, in case of vortex flow granulation, or satisfactorily sprayed, in case of fluidization spraying granulation, similarly to the granulating solvents. As to the concentration of the binding agents, experts of tablet manufacture have the corresponding experience. The amount of the microcrystalline cellulose is 5-30 % of the total mass of the granulating liquid.

Using the granulating liquid of the invention, the granulation process itself and from the granules obtained the tabletting are carried out in a manner known *per se*.

The process of the invention i.e. the novel use of microcrystalline cellulose according to the invention is a significant progress in the field of granulation technologies since the microcrystalline cellulose particles applied to the surface of the particles of the materials to be granulated from the

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suspension form a layer thereon thereby improving the compressing and lubrication (friction) properties of the particles. Consequently, the quantity of binding agents and glidents can be reduced in the composition and suitable tablet strength as well as fast dissolution of the active ingredient are obtained.

Thus, the use of the process of the invention has to be taken into consideration primarily for active ingredients that "stick" in tabletting or the dissolution rate of which is significantly reduced by the polymeric binding agents employed. The first group includes active ingredients like metoprolol tartrate [1-[4-(2methoxymethyl)phenoxy]-3-[(1-methylethyl)amino]-2-propanol tartrate] and bencyclane fumarate [N,N-dimethyl-3-[1-(phenylmethyl)cycloheptyloxy]-1-propanamine fumaratel. In tabletting the granules thereof prepared by the conventional granulation process, sticking problems on the surface of the tablet as well as "drawing problems" on the side of the tablet are experienced. regularly. The second group includes e.g. hydrochlorothiazide [6-chloro-3,4-dihydro-2H-1,2,4-benzothiadiazine-7-sulfonamide 1,1-dioxide], ranitidine [N-2-[5-(dimethylaminomethyl)-2-furanylmethylthioethyl]-N'-methyl-2-nitro-1,1-ethenediamine], paracetamol [p-hydroxyacetanilide], deramciclane [N,Ndimethyl-2-[(1R,2S,4R)-2-phenyl-2-bornyloxy]ethylamine] etc. In case of using the binding agents in an amount that is needed to produce the required tablet strength, the dissolution of the latter active ingredients is very slow.

The invention is further elucidated by means of the following

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Examples.

Example 1

Preparation of tablets containing deramciclane

To prepare the granulating liquid, 45 g of hydroxypropyl methyl cellulose are dissolved in 900 ml of water, and, in the solution obtained, 48 g of microcrystalline cellulose grade 105 (90 % of which have a particle size that is lower than 25 μ m) are dispersed.

To prepare the granules, 126 g of deramciclane fumarate, 180 g of mannitol and 300 g of microcrystalline cellulose grade 101 (90 % of which have a particle size that is lower than 50 μ m) are transfered into the container of a fluidization granulating apparatus type Glatt GPCG 1, fluidized by introducing air at 40 °C, and the above granulating liquid is sprayed on the fluidized powder in about 20 minutes. The particles obtained are dried, and passed through a sieve having a mesh size of 1 mm. To the granules obtained, 54 g of sodium carboxymethyl cellulose (disintegrating agent), 18 g of talc (lubricant) and 9 g of magnesium stearate (lubricant) are added, and the mixture is tabletted to produce lentiform tablets of 9 mm diameter. Each tablet has a mass of 260 mg. During tabletting no signs indicating sticking were found either on the dies, or on the surface of the tablets.

The critical parameters of the tablets determined according to

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the relevant prescriptions of the European Pharmacopeia are as follows:

Compre ssing force	Wear in	Disinteg ration	Breaking strength in	Height in	Mass	Dissolution in %** after		n %**
in kN	%	in min	N	mm	in mg	5 min	15 min	30 min
8	0.23	3.97	66.7	4,35	260			
10	0.19	6.6	81.24	4.23	260			
12	0.19	7.33	93.31	4.18	262			
14	0.19	8.4	97.74*	4.16	263.1	41.65	86.15	92.34
16	0.19	8.55	106.5	4.13	265.5			
20	0.26	9.31	110.17	4.10	265.9			

^x The value of tensile strength: 2.61 MPa.

Taking into consideration the requirements given on page 8, the quality of the deramciclane tablets prepared is very favourable.

Example for comparison

For comparison, the deramciclane tablets were prepared by using a granulating liquid that did not contain any microcrystalline cellulose, while the amount of microcrystalline cellulose in the powder mixture was increased correspondingly. In tabletting, the surface of the lower press die became dull indicating the adherence of a thin layer, thus, the sticking of the composition.

The critical parameters of the tablets determined according to

^{**} The dissolution rate is not prescribed in the European Pharmacopeia.

the relevant prescriptions of the European Pharmacopeia are as follows:

Compres	Wear		Breaking	Height	Mass	Dissolution in %**		า %**
sing	in	ration	strength	in			after	
force			in					
in kN	%	in min	N	mm	in mg	5 min	15 min	30 min
8	0.19	1.55	46.7	4.50	264.9			
10	0.15	2.30	59.4	4.33	263.6			
12	0.23	2.82	67.0	4.25	263.4			
14	0.19	3.53	74.6*	4.22	265.4	73.71	95.89	98.79
16	0.19	3.73	79.5	4.13	261.0			
20	0.27	4.10	86.4	4.10	262.8			

^x The value of tensile strength: 1.96 MPa.

As to the physical parameters of the tablets obtained, the breaking strength and disintegration time are lower, and, correspondingly, the dissolution rate is somewhat higher than those of tablets obtained in Example 1. However, the appearance of the tablets is not suitable owing to the sticking to the dies.

Example 2

Preparation of tablets containing hydrochlorothiazide

1.5 kg of lactose are dissolved in 6000 ml of water warmed to 60-70 °C, and, in the solution obtained, 1.5 kg of microcrystalline cellulose grade 105 are suspended. During use, the suspension is maintained at 60-70 °C.

^{xx} The dissolution rate is not prescribed in the European Pharmacopeia.

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7.5 kg of hydrochlorothiazide are fluidized in a fluidization granulating apparatus type Aeromatic STE 15 using air stream at 60±5 °C, and the granulating liquid prepared above is sprayed on the active ingredient at 200 ml/min feeding velocity and under 1.5 bar spraying pressure. Then the granules are dried until the wet content is not higher than 1 % by mass, and passed through a sieve having a mesh size of 1 mm.

The granules obtained can be diluted with carriers conventionally used in direct tabletting and/or with active ingredients having blood pressure lowering effect or the granules thereof, then compressed to obtain tablets containing one or more active ingredients.

To prepare a combination composition wherein each tablet contains 15 mg of hydrochlorothiazide and 50 mg of captopril [(S)-1-(3-mercapto-2-methyl-1-oxopropyl)-L-proline], 1.05 kg of the above granules, furthermore 2.50 kg of captopril, 4.85 kg of spray dried lactose monohydrate, 4.85 kg of microcrystalline cellulose grade 102, 1.50 kg of maize starch, 0.15 kg of stearine and 0.05 kg of magnesium stearate are transferred into a gravity mixer of 50 litre capacity, homogenized for 25 minutes, then compressed to 300 mg tablets by a rotary tabletting machine Manesty Betapress using flat flanged press dies of 10 mm diameter. Each tablet obtained contains 15 mg of hydrochlorothiazide and 50 mg of captopril.

To prepare a combination composition wherein each tablet

contains 25 mg of hydrochlorothiazide and 25 mg of captopril, 1.750 kg of the above granules, furthermore 1.250 kg of captopril, 2.425 kg of spray dried lactose monohydrate, 2.425 kg of microcrystalline cellulose grade 102, 0.750 kg of maize starch, 0.075 kg of stearine and 0.025 kg of magnesium stearate are transfered into into a gravity mixer of 30 litre capacity, homogenized for 25 minutes, then compressed to 174 mg tablets by a rotary tabletting machine Manesty Betapress using flat flanged press dies of 8 mm diameter or lentiform and engraved or divided dies. Each tablet obtained contains 25 mg of hydrochlorothiazide and 25 mg of captopril.

3 further batches were manufactured from each latter tablet composition, and the critical parameters of the tablets obtained were as follows. The tablet parameters were determined according to the relevant prescriptions of the US Pharmacopeia.

Requirement for dissolution of the USP: dissolution of the active ingredients using 6 tablets for the determination:

captopril after 20 min not lower than 85 %, hydrochlorothiazide after 20 min not lower than 65 %.

	Batch No. 1	Batch No. 2	Batch No. 3
0.284-0.314	0.3096	0.3062	0.3034
3.10-3.50	3.30	3.32	3.25
± 5	-2.2; +3.3	-1.4 ; +2.0	-2.0; +3.4
min. 35	51	43	48
min. 1	1.54	1.29	1.47
1	0.01	0.06	0.03
	103.0– 106.1 97.1– 98.4	104.4– 106.7 88.7–93.0	96.8– 101.4 75.0– 87.0
	3.10–3.50 ± 5 min. 35	0.284-0.314	0.284-0.314

Captopril/hydro- chlorothiazide tablet 25/25 mg	Requirement	Batch No. 1	Batch No. 2	Batch No. 3
Average mass in g	0.161- 0.1871	0.1757	0.1750	0.1766
Height in mm	2.73-3.07	2.96	2.94	2.93
Mass deviation in %	± 5	-1.0; +2.8	-4.6 ; +2.3	-2.7; +2.0
Breaking strength in N	min. 30	33	36	42
Tensile strength in MPa	min. 1	1.39	1.53	2.04
Wear loss in %	max. 1	0.04	0.03	0.07
Dissolution of the active ingredient in % captopril after 10 min hydrochlorothiazide after 10 min		101.7– 105.3 94.7– 100.3	102.3– 106.4 99.5– 105.3	103.7- 107.2 102.1- 107.5

Thus, according to the test results, tablets having good mechanical strength could be produced. From the tablets obtained, the active ingredients could be dissolved significantly faster than prescribed by the US Pharmacopeia.

Example 3

Preparation of tablets containing ranitidine

1.05 kg of microcrystalline cellulose grade 105 are suspended in a mixture of 7000 ml of 95 % by volume of ethanol and 1000

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ml of water. The materials to be granulated (11.76 kg of ranitidine hydrochloride and 3.08 kg of microcrystalline cellulose grade 105) are homogenized in a vortex flow granulation equipment Diosna of 100 litre capacity for about 3 minutes. The above granulating suspension is added in about 5 minutes under constant stirring, and the granulation procedure is carried out for further 12 minutes. The wet particles are dried in a fluidization granulating apparatus type Aeromatic STE 15, the dry granules are regranulated by passing them through a sieve having a mesh size of 0.8 mm, and the granules obtained are homogenized with 3.50 kg of microcrystalline cellulose grade 102, 1.05 kg of sodium carboxymethyl cellulose and a mixture of 0.14 kg of magnesium stearate and 0.07 kg of silica in a gravity mixer of 100 litre capacity. From the homogenized mixture, 295 mg lentiform tablets of 10 mm diameter are prepared using a rotary tabletting machine Manesty Betapress or 590 mg oviform tablets of 17.5 mm length and 7.5 mm width are produced by a tabletting machine Kilian RTS 21. The tablets obtained contain 150 mg and 300 mg of ranitidine, respectively.

The critical parameters of the tablets obtained were as follows. The tablet parameters were determined according to the relevant prescriptions of the US Pharmacopeia.

Requirement for dissolution of the USP: dissolution of the active ingredient using 6 tablets for the determination:

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in 45 minutes not less than 85 %.

Ranitidine tablet	150 mg	150 mg	300 mg	300 mg
Parameter	Requiremen t	Value determined	Requirement	Value determi ned
Average mass in g	0.2803- 0.3097	0.2934	0.5605 - 0.6195	0.5870
Mass deviation in %	±5	-2.1; +2.5	-1.9 ; +1.5	-2.0; +3.4
Height in mm	4.14-4.66	4.50	4.79–5.41	5.04
Breaking strength in N	min. 60 N	105	min. 100 N	159
Tensile strength in Mpa	min. 1	2.33	min. 1	1.80
Wear loss in %	max. 1	0,0	max. 1	0.0

The tablets were coated with a film based on 12 mg and 24 mg of water-soluble hydroxypropyl methyl cellulose, respectively, then the dissolution rate was determined according to the prescription of the USP. The following values were obtained:

Dissolution of the active	in case of the	in case of the	
ingredient in	150 mg tablet	300 mg tablet in	
	in % by weight	% by weight	
15 min.	85.5-90.0	76.0-85.4	
30 min.	92.9-99.6	94.5-100.9	

Thus, based on the test data, tablets having very good mechanical strength could be prepared from which the dissolution of the active ingredient is significantly faster than prescribed by the USP.

Example 4 Preparation of tablets containing metoprolol

3.2 kg of poly(vinyl pyrrolidone) are dissolved in a mixture of 17 litre of water and 17 litre of 95 % by volume of ethanol, and, in the solution obtained, 4.8 kg of microcrystalline cellulose grade 105 are suspended. The materials to be granulated (40.0 kg of metoprolol tartrate, 61.60 kg of microcrystalline cellulose grade 105, 12.0 kg of sodium carboxymethyl starch, 1.6 kg of silica) are homogenized in a vortex flow granulation equipment Diosna of 400 litre capacity for about 3 minutes. The above granulating suspension is added in about 1-2 minutes under constant stirring, and the granulation procedure is carried out for further 10 minutes. The wet particles are dried in a fluidization granulating apparatus type Glatt WSG 120, the dry granules are regranulated by passing them through a sieve having a mesh size of 0.8 mm, and the granules obtained are homogenized

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with a mixture of 3.2 kg of magnesium stearate and 1.6 kg of silica in a gravity mixer of 450 litre capacity.

From the homogeneous mixture 80, 160 and 320 mg tablets can be compressed on a rotary tabletting machine (e.g. Manesty Betapress, Kilian T300 A100, Fette Perfecta 300 etc.) using flat flanged or lentiform and engraved or divided dies of 6 mm, 8 mm and 10 mm diameter. The above tablets contain 25 mg, 50 mg and 100 mg of metoprolol tartrate, respectively.

3 further batches were manufactured from each latter tablet composition, and the critical parameters of the tablets obtained were as follows. The tablet parameters were determined according to the relevant prescriptions of the US Pharmacopeia.

Requirement for dissolution of the USP: dissolution of the active ingredient using 6 tablets for the determination:

after 30 min

not lower than 80 %.

Metoprolol tablet 25 mg	Require- ment	Batch No. 1	Batch No. 2	Batch No. 3
Average mass in g	0.072-0.088	0.0826	0.0809	0.0812
Mass deviation in %	± 10	-4.6; +5.3	-2.1 ; +3.4	-1.2; +1.7
Height in mm	2.71-3.19	2.85	2.87	2.86
Breaking strength in N	min. 20	35	36	38
Tensile strength in Mpa	min. 1	2.04	2.09	2.21
Wear loss in %	max.1	0.11	0.12	0.11
Dissolution of the active ingredient in % after 10 min		98.2- 104.4	94.8- 102.3	96.1- 100.5

Metoprolol tablet 50 mg	Require- ment	Batch No. 1	Batch No. 2	Batch No. 3	
Average mass in g	0.148-0.172	0.1605	0.1605	0.1597	
Mass deviation in %	± 10	-2.5; +3.3	-2.5 ; +1.6	-1.7; +3.2	
Height in mm	3.10-3.50	3.27	3.24	3.25	
Breaking strength in N	min. 30	40	40	46	
Tensile strength in Mpa	min. 1	1.52	1.54	1.76	
Wear loss in %	max.1	0.00	0.00	0.00	
Dissolution of the active ingredient in % After 10 min		91.7- 107.1	95.5- 101.3	88.7-90.2	

Metoprolol tablet	Require- ment	Batch No. 1	Batch No. 2	Batch No. 3
Average mass in g	0.304-0.336	0.3242	0.321	0.3233
Mass deviation in	± 10	-2.1; +2.2	-1.7 ; +2.2	-3.5; +3.0
Height in mm	3.95-4.45	4.37	4.27	4.28
Breaking strength in N	min. 40	44	45	51
Tensile strength in MPa	min. 1	1.01	1.05	1.19
Wear loss in %	max.1.0	0.03	0.06	0.06
Dissolution of the active ingredient in % after 10 min		91.6-97.6	89.35- 91.93	95.0- 101.1

Thus, based on the test data, tablets having very good mechanical strength could be prepared from which the dissolution of the active ingredient is significantly faster than prescribed by the USP.

Example 5

Preparation of tablets containing deramciclane

To prepare the granulating liquid, 192 g of poly(vinyl pyrrolidone) are dissolved in 720 ml of water, and, in the solution obtained, 120 g of microcrystalline cellulose grade 105 (90 % of which have a particle size that is lower than 25 μ m) are dispersed.

To prepare the granules, 504 g of deramciclane fumarate, 360 g of mannitol and 480 g of microcrystalline cellulose grade 101 (90 % of which have a particle size that is lower than 50 μm) are transfered into the container of a fluidization granulating apparatus type Glatt GPCG 1, fluidized by introducing air at 40 °C, and the above granulating liquid is sprayed on the fluidized powder in about 23 minutes. The particles obtained are dried, and passed through a sieve having a mesh size of 1 mm. To the granules obtained, 120 g of sodium carboxymethyl cellulose (disintegrating agent) and 24 g of magnesium stearate are added, and the mixture is tabletted to produce lentiform tablets of 7 mm diameter using a Manesty Betapress tabletting machine. Each tablet has a mass of 150 mg ± 5 % and contains 30 mg of deramciclane base. During tabletting no signs indicating sticking were found either on the dies, or on the surface of the tablets.

The critical parameters of the tablets determined according to the relevant prescriptions of the European Pharmacopeia are as follows:

Compre ssing force	Wear in	Disinte gration	Breakin g strength in	Height in	Mass	Dissolution in %* after		
in kN	%	in min	N	mm	in mg	5 min	15 min	30 min
6	0.08	8.2	39.5	4.48	148,7			
8	0.10	9.1	49.5	4.38	148.3			
10	0.05	9.3	53.6	4.36	148.0		-	
11	0.09	9.2	53.9	4.34	148.9	39.7	82.8	95.6
12	0.02	9.8	55.5	4.40	151.5			

Dissolution test was carried out in 900 ml of buffer having a pH value of 6.8 and using a bladed device at 50 revolution/min.

Taking into consideration the requirements given on page 8, the quality of the deramciclane tablets prepared is very favourable.

Example 6

Preparation of tablets containing deramciclane

To prepare the granulating liquid, 192 g of poly(vinyl pyrrolidone) are dissolved in 700 ml of water, and, in the solution obtained, 120 g of microcrystalline cellulose grade 105 (90 % of which have a particle size that is lower than 25 μ m) are dispersed.

To prepare the granules, 504 g of deramciclane fumarate, 360 g of mannitol and 480 g of microcrystalline cellulose grade 101 (90 % of which have a particle size that is lower than 50 μm) are transfered into the container of a fluidization granulating apparatus type Glatt GPCG 1, fluidized by introducing air at 40 °C, and the above granulating liquid is sprayed on the fluidized powder in about 20 minutes. The particles obtained are dried, and passed through a sieve having a mesh size of 1 mm. To the granules obtained, 120 g of sodium carboxymethyl cellulose (disintegrating agent), 120 g of microcrystalline cellulose grade 102 (90 % of which have a particle size that is lower than 90 μm) and 36 g of magnesium stearate are added, and the mixture is tabletted to produce lentiform tablets of 10 mm

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diameter using a Manesty B3B tabletting machine. Each tablet has a mass of 320 mg and contains 60 mg of deramciclane base. During tabletting no signs indicating sticking were found either on the dies, or on the surface of the tablets.

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Claims:

1. A process for the preparation of tablets that can be well compressed and have good mechanical strength from pharmaceutically active ingredient(s) having unfavourable tabletting properties by admixing the pharmaceutically active ingredient(s) to conventional carriers used in tabletting, preferably binding agent(s) and/or filling agent(s) and/or disintegrating agent(s) and/or surfactant(s), granulating the mixture in the presence of a granulating liquid by a kneading or a fluidization spraying process, and tabletting the granules obtained using further carriers conventionally employed in tabletting, preferably lubricant(s) and/or disintegrating agent(s) and/or glident(s),

in which

the granulating liquid is a suspension of 5-30 % of microcrystalline cellulose - 90 % of which have a particle size that is lower than 50 μ m, and the amount of the microcrystalline cellulose refers to the final tablet mass - in water and/or ethanol and/or isopropanol, and said suspension may contain also a part of the ingredients of the granules in dissolved form.

- A process as claimed in Claim 1, in which
 % of the microcrystalline cellulose suspended in the granulating liquid have a particle size that is lower than 25 μm.
- 3. A process as claimed in Claim 1 or 2, in which the granulating liquid contains in addition to the

microcrystalline cellulose - poly(vinyl pyrrolidone), hydroxypropyl methyl cellulose, hydroxypropyl cellulose, ethyl cellulose and/or gelatin as binding agent in dissolved form.

- 4. A process as claimed in Claim 1 or 2, in which the granulating liquid contains in addition to the microcrystalline cellulose lactose, mannitol and/or glucose as filling agent in dissolved form.
- 5. A process as claimed in any of Claims 1-4, in which the active ingredient is deramciclane or a pharmaceutically acceptable acid addition salt thereof.
- 6. Tablets as prepared by the process claimed in Claim 5 having high breaking strength and disintegration time.
- 7. Tablets as claimed in Claim 6 having a breaking strength of above 90 N.
- 8. Tablets as claimed in Claim 6 having a disintegration time of 5-9 minutes.

INTERNATIONAL SEARCH REPORT

PCT/HU 02/00035

a. classification of subject matter IPC 7 A61K9/16 A61K9/20								
According to International Patent Classification (IPC) or to both national classification and IPC								
B. FIELDS SEARCHED								
Minimum documentation searched (classification system followed by classification symbols) IPC 7 A61K								
Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched								
Electronic data base consulted during the international search (name of data base and, where practical, search terms used)								
EPO-Internal, WPI Data, PAJ, BIOSIS, MEDLINE, PASCAL, EMBASE, CHEM ABS Data								
C. DOCUMENTS CONSIDERED TO BE RELEVANT								
Category °	Citation of document, with indication, where appropriate, of the rel	Relevant to claim No.						
А	EP 0 958 812 A (FREUNT IND CO LTI 24 November 1999 (1999-11-24) page 5, line 33 - line 38; examp	1-8						
А	WO 98 36737 A (LUHADIYA ASHOK PRI ;PROCTER & GAMBLE (US)) 27 August 1998 (1998-08-27) page 7, line 11 - line 20	1-8						
А	VOIGT ET AL: "Pharmazeutische Tefür Studium und Beruf" 1993 , PHARMAZEUTISCHE TECHNOLOG STUDIUM UND BERUF, XX, XX, PAGE(XP002900619 page 208, paragraph 4 page 212, last paragraph	1-8						
Further documents are listed in the continuation of box C. Patent family members are listed in annex.								
Special categories of cited documents:								
'A' docum	ent defining the general state of the art which is not dered to be of particular relevance	or priority date and not in conflict with cited to understand the principle or th invention						
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other	means ent published prior to the international filing date but	ments, such combination being obvious to a person skilled in the art.						
	than the priority date claimed actual completion of the international search	&" document member of the same patent family Date of mailing of the international search report						
	31 July 2002	09/08/2002						
Name and	mailing address of the ISA	Authorized officer						
	European Patent Office, P.B. 5818 Patentlaan 2 NL – 2280 HV Rijswijk Tel. (+31-70) 340–2040, Tx. 31 651 epo nl, Fax: (+31-70) 340–3016	Zimmer, B						

INTERNATIONAL SEARCH REPORT

Information on patent family members

PCT/HU 02/00035

Patent document cited in search report		Publication date		Patent family member(s)	Publication date
EP 0958812	A	24-11-1999	JP EP US WO	10139659 A 0958812 A1 6171619 B1 9810751 A1	26-05-1998 24-11-1999 09-01-2001 19-03-1998
WO 9836737	A	27-08-1998	WO AU JP	9836737 A1 1970797 A 11506473 T	27-08-1998 09-09-1998 08-06-1999

IDS REFERENCES

